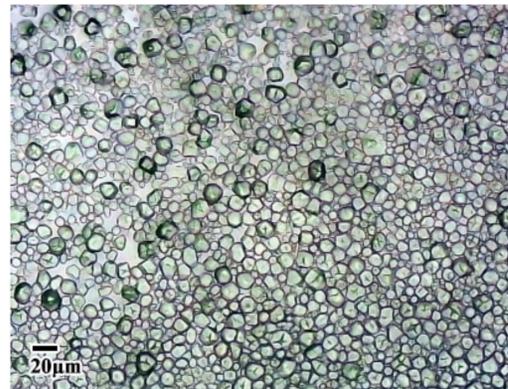


*New perspectives on the mechanism of shear thickening*

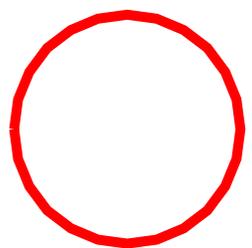
Helen J. Wilson

Department of Mathematics, UCL



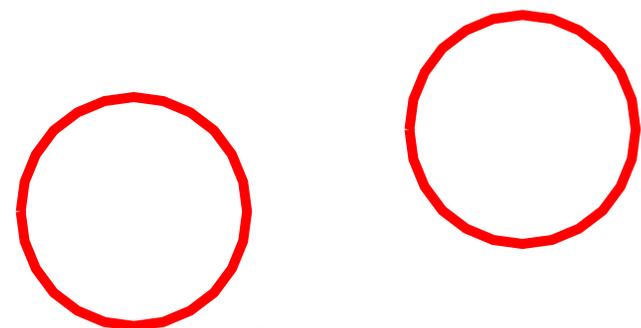
# Model Suspensions in Shear: Definitions

---



Viscous fluid  
 Viscosity  $\mu$   
 Density  $\rho$

Solid particles, radius  $a$



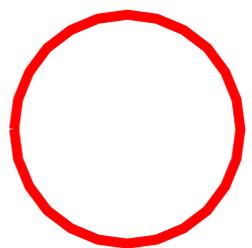
Shear flow, rate  $\dot{\gamma}$

Particles are identical, spherical, **non-colloidal**: large enough to neglect Brownian Motion.

Reynolds number  $Re = \rho \dot{\gamma} / \mu \ll 1$   
 Solid volume, area fraction  $\phi, c$

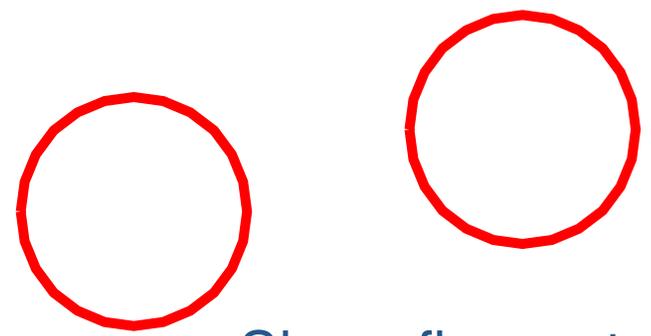
# Model Suspensions in Shear: Definitions

---



Viscous fluid  
 Viscosity  $\mu$   
 Density  $\rho$

Solid particles, radius  $a$



Shear flow, rate  $\dot{\gamma}$

Particles are identical, spherical, **non-colloidal**: large enough to neglect Brownian Motion.

Reynolds number  $Re = \rho \dot{\gamma} / \mu \ll 1$

Solid volume, area fraction  $\phi, c$

## Key Questions:

- What is the macroscopic **viscosity**?
- What are the **normal stress differences**?

## Background: Stokes Flow

---

Governing equations for Newtonian fluid mechanics are the **Navier-Stokes** equations. When  $Re \ll 1$  and with no body forces they reduce to the **Stokes Equations**:

$$\sigma = -p\mathbf{I} + \mu \left( \nabla \mathbf{u} + \nabla \mathbf{u}^T \right) \quad \nabla \cdot \mathbf{u} = 0 \quad \nabla \cdot \sigma = \mathbf{0}$$

$p$  = pressure

$\mathbf{u}$  = velocity

$\sigma$  = stress

## Background: Stokes Flow

---

Governing equations for Newtonian fluid mechanics are the **Navier-Stokes** equations. When  $Re \ll 1$  and with no body forces they reduce to the **Stokes Equations**:

$$\sigma = -p\mathbf{I} + \mu \left( \nabla \mathbf{u} + \nabla \mathbf{u}^\top \right) \quad \nabla \cdot \mathbf{u} = 0 \quad \nabla \cdot \sigma = \mathbf{0}$$

$p$  = pressure

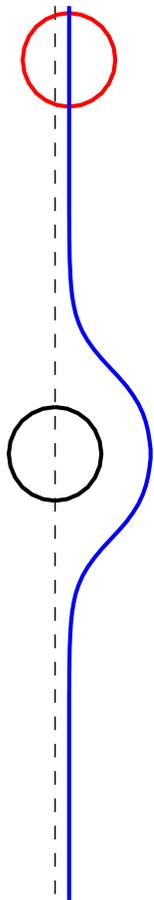
$\mathbf{u}$  = velocity

$\sigma$  = stress

- Linear equations
  - Flow vector  $\mathbf{u}$  depends linearly on boundary data
- Quasi-static (no  $\partial/\partial t$  term)
  - $\mathbf{u}$  responds instantly to any changes; history irrelevant
- Reversible
  - Reverse boundary data/forcing,  $\mathbf{u} \rightarrow -\mathbf{u}$  and all trajectories backtrack

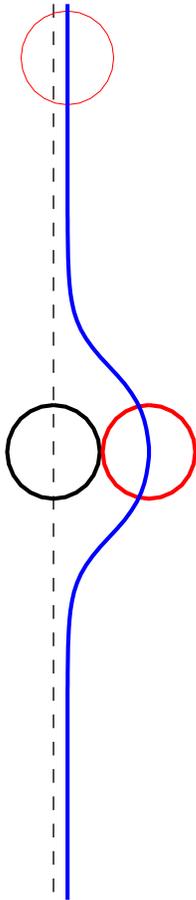
## Background: Experimental Evidence of Contact

---



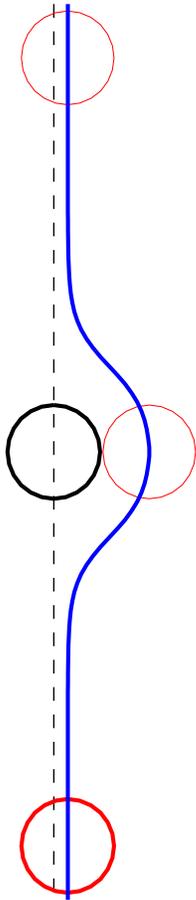
# Background: Experimental Evidence of Contact

---



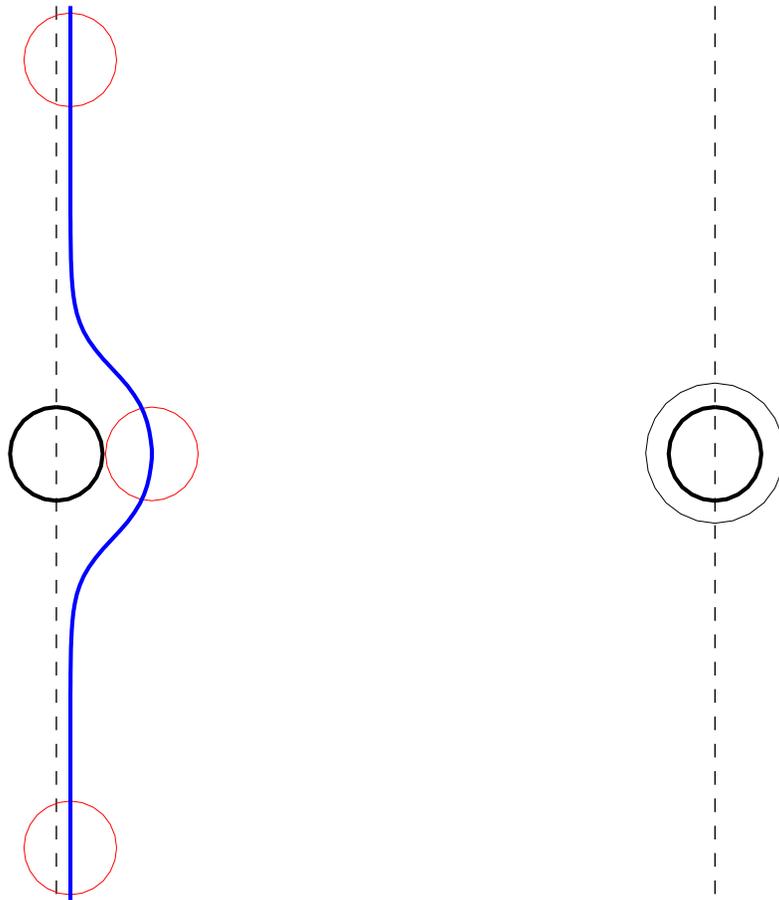
# Background: Experimental Evidence of Contact

---



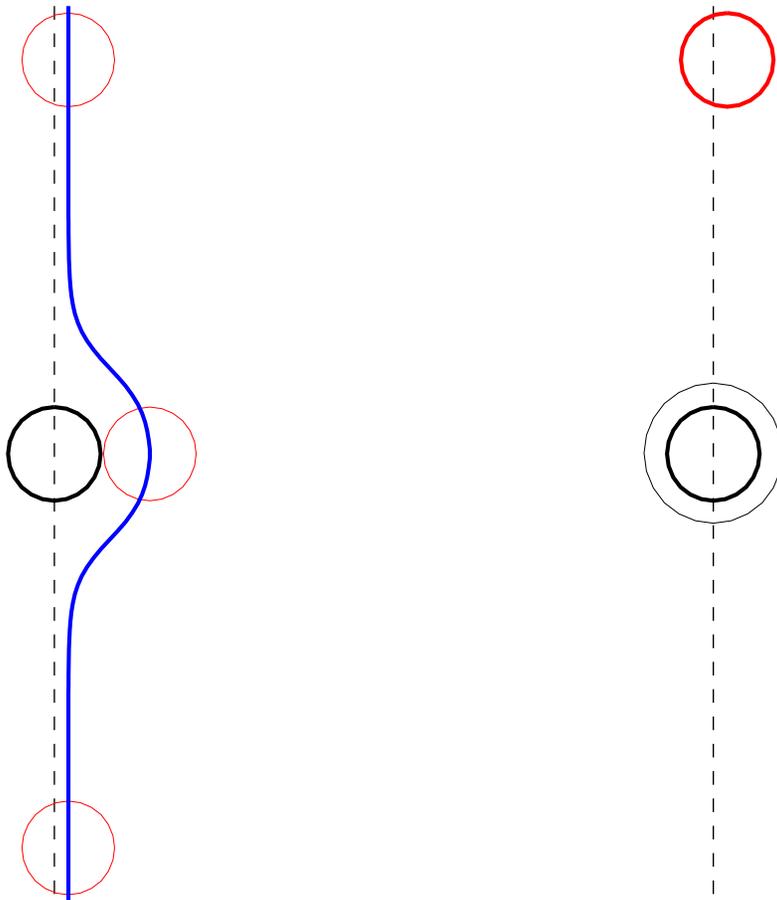
# Background: Experimental Evidence of Contact

---



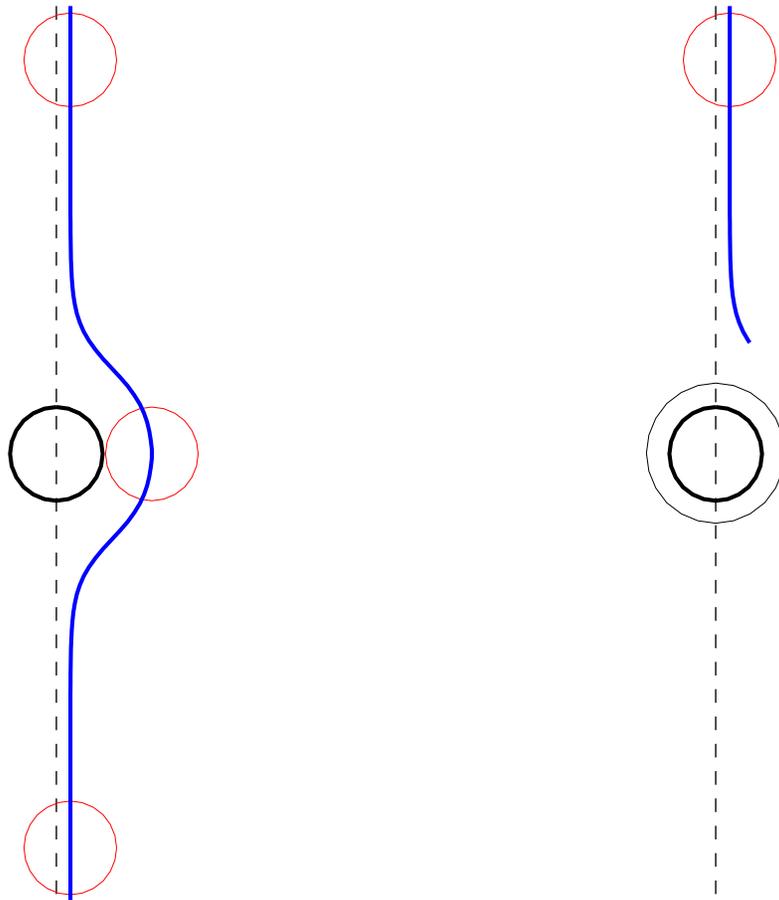
# Background: Experimental Evidence of Contact

---



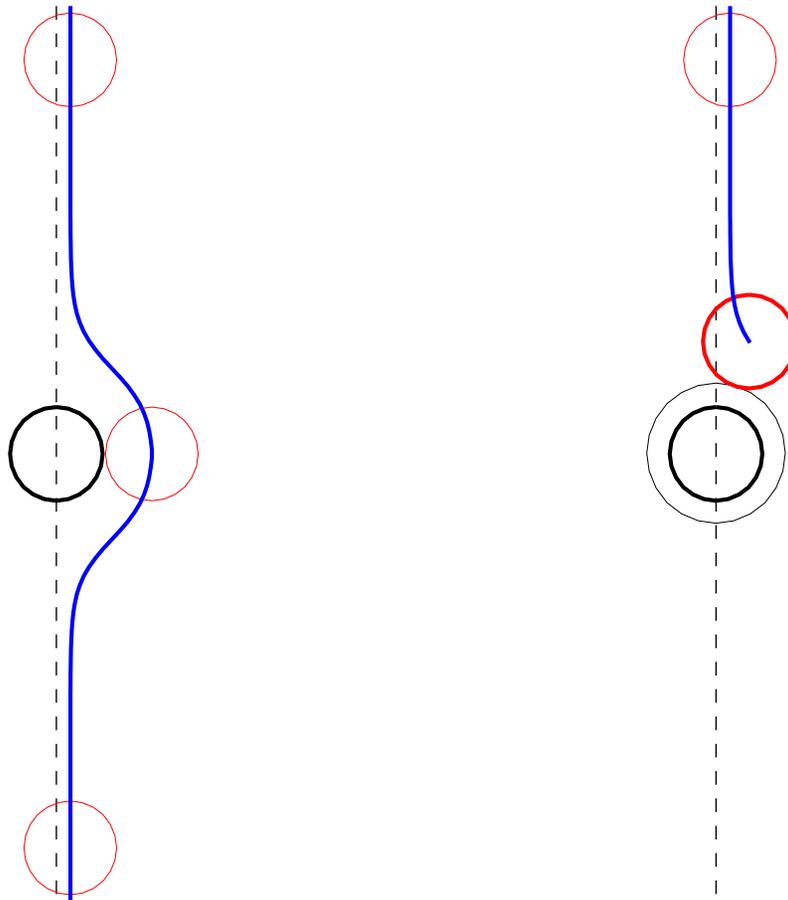
# Background: Experimental Evidence of Contact

---



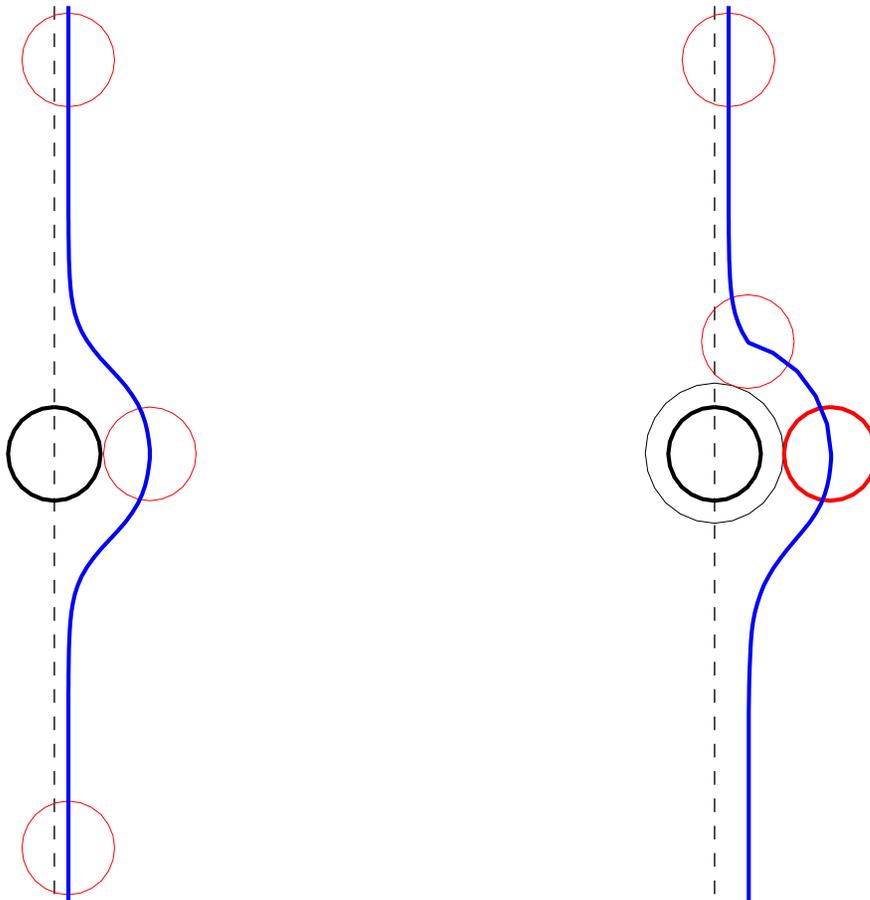
# Background: Experimental Evidence of Contact

---



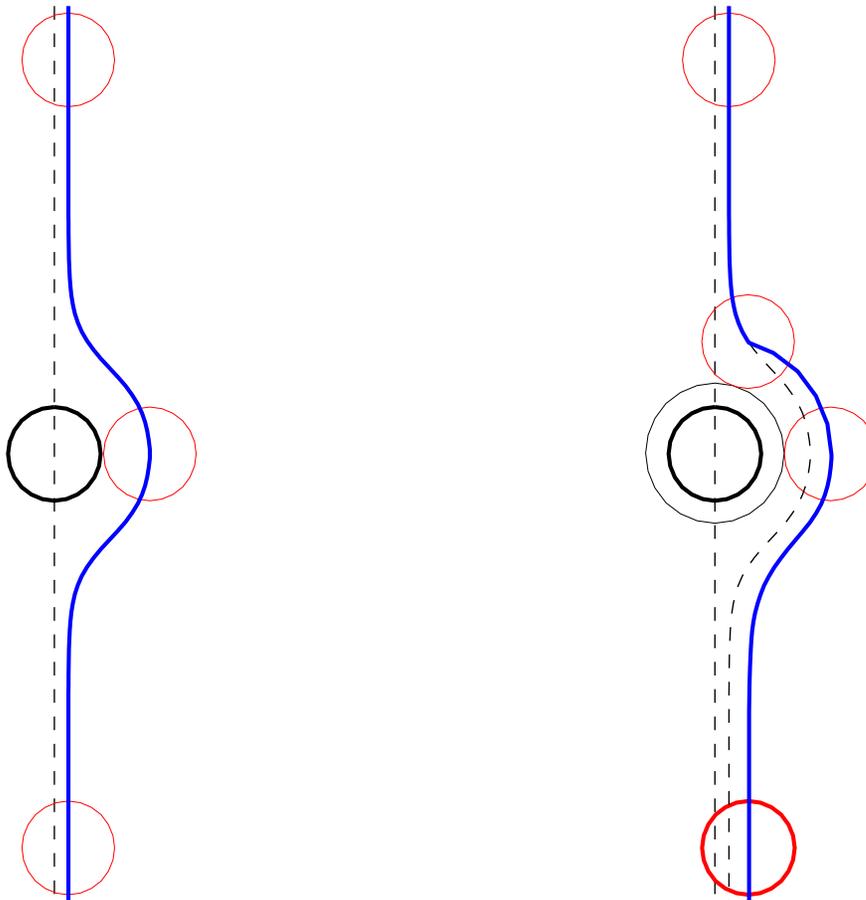
# Background: Experimental Evidence of Contact

---



# Background: Experimental Evidence of Contact

---

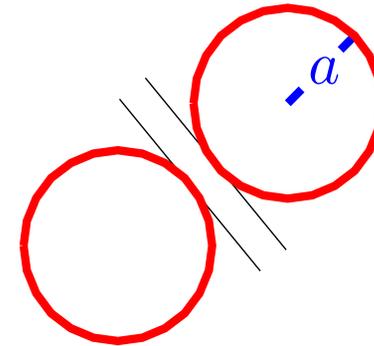


# Simple Models of Contact

---

## Dimensionless roughness height $\xi$

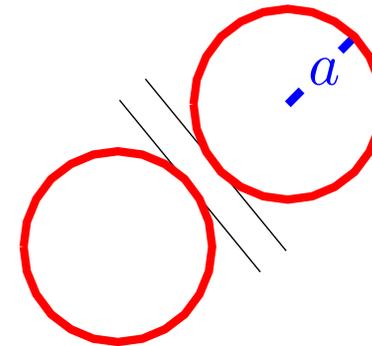
- Hydrodynamics unaffected
- Approach closer than  $\xi a$  prevented by normal contact force  $F_n$
- Particles free to separate



# Simple Models of Contact

## Dimensionless roughness height $\xi$

- Hydrodynamics unaffected
- Approach closer than  $\xi a$  prevented by normal contact force  $F_n$
- Particles free to separate



## Coefficient of friction $\nu$

- Applies tangential friction force  $F_t$
- Rolling contact if  $F_n$  large enough:  $|F_t| \leq \nu |F_n|$  and no relative motion at contact point
- Slipping contact otherwise:  $|F_t| = \nu |F_n|$  and particles roll and slide past one another
- **Extra:** critical load  $F_c$ : friction applied only if  $|F_n| > F_c$

## History: Dilute Suspensions

---

‘Expand’ about the state of no particles at all:

- $\phi = 0$ , Newtonian fluid with viscosity  $\eta = \mu$ .
- Einstein (1906 & 1915) calculated stress to order  $\phi$   
 Single free solid sphere at the origin of a flow field  
 $\mathbf{U} = \mathbf{U}^\infty + \boldsymbol{\Omega} \times \mathbf{x} + \mathbf{E} \cdot \mathbf{x}$  causes extra dissipation (stresslet)

$$\mathbf{S} = \frac{20}{3} \pi \mu a^3 \mathbf{E}.$$

## History: Dilute Suspensions

---

‘Expand’ about the state of no particles at all:

- $\phi = 0$ , Newtonian fluid with viscosity  $\eta = \mu$ .
- Einstein (1906 & 1915) calculated stress to order  $\phi$   
 Single free solid sphere at the origin of a flow field  
 $\mathbf{U} = \mathbf{U}^\infty + \boldsymbol{\Omega} \times \mathbf{x} + \mathbf{E} \cdot \mathbf{x}$  causes extra dissipation (stresslet)

$$\mathbf{S} = \frac{20}{3} \pi \mu a^3 \mathbf{E}.$$

The whole stress for the suspension is

$$\boldsymbol{\Sigma} = -p\mathbf{I} + 2\mu \left( 1 + \frac{5}{2}\phi \right) \mathbf{E}.$$

## History: Dilute Suspensions

---

‘Expand’ about the state of no particles at all:

- $\phi = 0$ , Newtonian fluid with viscosity  $\eta = \mu$ .
- Einstein (1906 & 1915) calculated stress to order  $\phi$   
 Single free solid sphere at the origin of a flow field  
 $\mathbf{U} = \mathbf{U}^\infty + \boldsymbol{\Omega} \times \mathbf{x} + \mathbf{E} \cdot \mathbf{x}$  causes extra dissipation (stresslet)

$$\mathbf{S} = \frac{20}{3} \pi \mu a^3 \mathbf{E}.$$

The whole stress for the suspension is

$$\boldsymbol{\Sigma} = -p\mathbf{I} + 2\mu \left( 1 + \frac{5}{2}\phi \right) \mathbf{E}.$$

The suspension is a Newtonian fluid with this **viscosity**.

## History: Dilute Suspensions

---

Batchelor & Green (1972) calculated stress to order  $\phi^2$  for smooth spheres

- A pair of particles at positions  $\mathbf{x}$  and  $\mathbf{x} + \mathbf{r}$  in the linear flow field cause the stresslets they would each cause alone plus an extra interaction stresslet

$$\mathbf{S}(\mathbf{r})$$

- The probability of finding a pair in this arrangement can be calculated using **trajectory analysis**; fine as long as all trajectories come from infinity
- The total extra stress at order  $\phi^2$  is calculated from

$$\int \mathbf{S}(\mathbf{r})P(\mathbf{r}) \, d\mathbf{r}.$$

## History: Dilute Suspensions

---

Batchelor & Green's calculation (1972) to order  $\phi^2$

- In **shear flow**  $\mathbf{U} = (\dot{\gamma}y, 0, 0)$ , not all particle trajectories come from infinity: there are **closed orbits** where  $\mathbb{P}$  cannot be found.

## History: Dilute Suspensions

---

### Batchelor & Green's calculation (1972) to order $\phi^2$

- In **shear flow**  $\mathbf{U} = (\dot{\gamma}y, 0, 0)$ , not all particle trajectories come from infinity: there are **closed orbits** where  $\mathbf{P}$  cannot be found.
- In the absence of any forces except hydrodynamics,  $\mathbf{P}$  is spherically symmetric

## History: Dilute Suspensions

---

### Batchelor & Green's calculation (1972) to order $\phi^2$

- In **shear flow**  $\mathbf{U} = (\dot{\gamma}y, 0, 0)$ , not all particle trajectories come from infinity: there are **closed orbits** where  $\mathbf{P}$  cannot be found.
- In the absence of any forces except hydrodynamics,  $\mathbf{P}$  is spherically symmetric
- By symmetry,  $N_1$  and  $N_2$  are zero so stress is Newtonian to  $O(\phi^2)$
- Viscosity  $\eta$  cannot be calculated: unknown quantity of particles  $\mathbf{P}$  on bound trajectories

## Effect of Contact: Dilute Suspensions

---

### Batchelor theory for smooth spheres

- Calculate stress from

$$\int \mathbf{S}(\mathbf{x}_0, \mathbf{x}_0 + \mathbf{r}) P(\mathbf{r}) d^3 \mathbf{r}$$

## Effect of Contact: Dilute Suspensions

---

### Batchelor theory for smooth spheres

- Calculate stress from

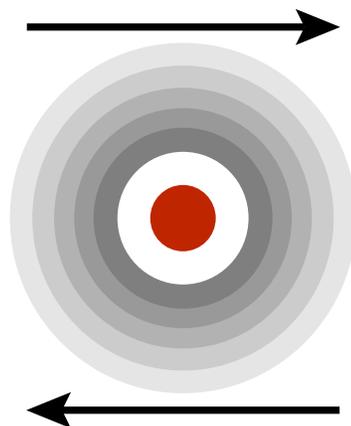
$$\int \mathbf{S}(\mathbf{x}_0, \mathbf{x}_0 + \mathbf{r}) P(\mathbf{r}) d^3 \mathbf{r}$$

### Perturbation by contact

- Stresslet  $\mathbf{S}$  hardly changes
- Pair distribution  $P$  of spheres strongly affected

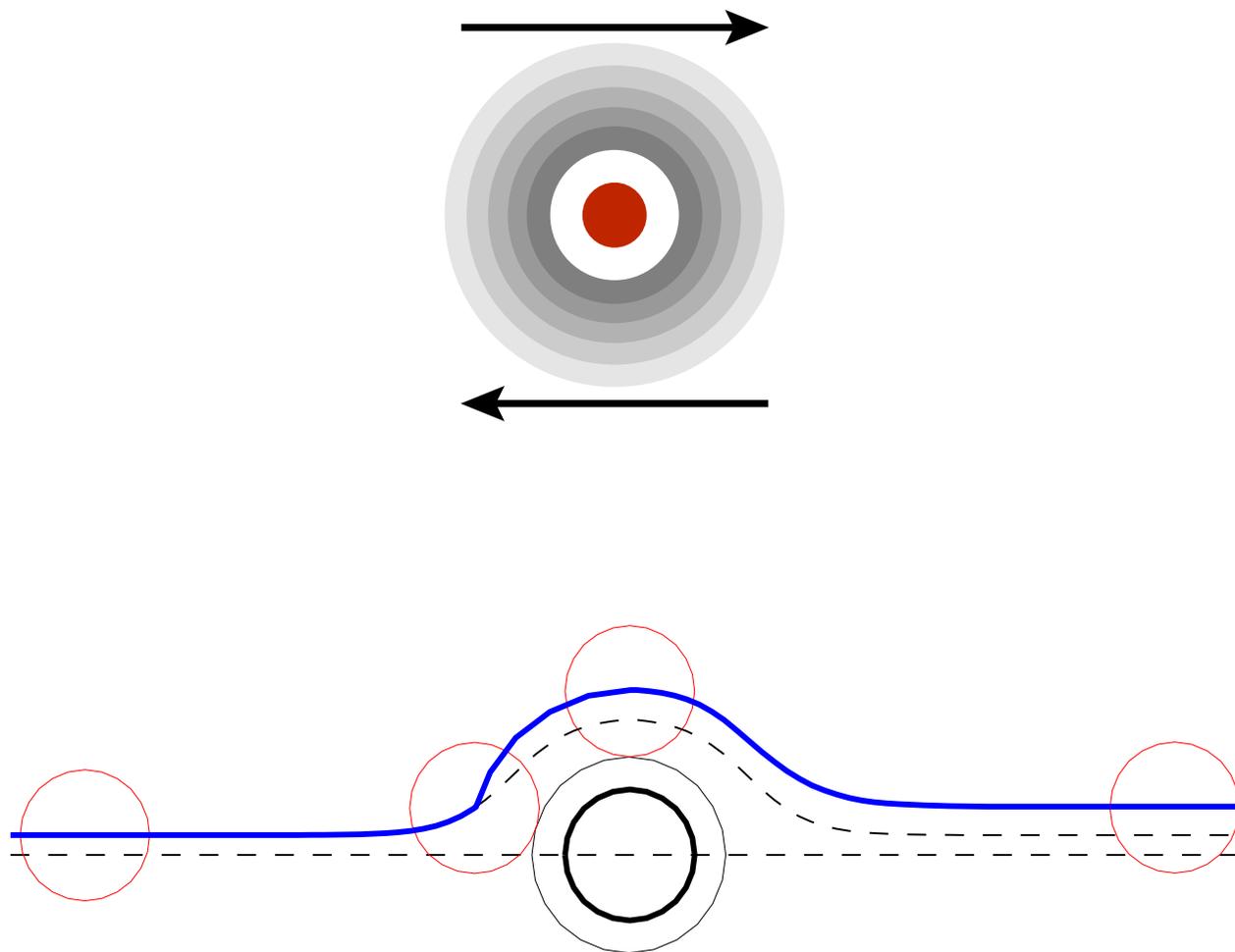
## Effect of Contact: Dilute Suspensions

---



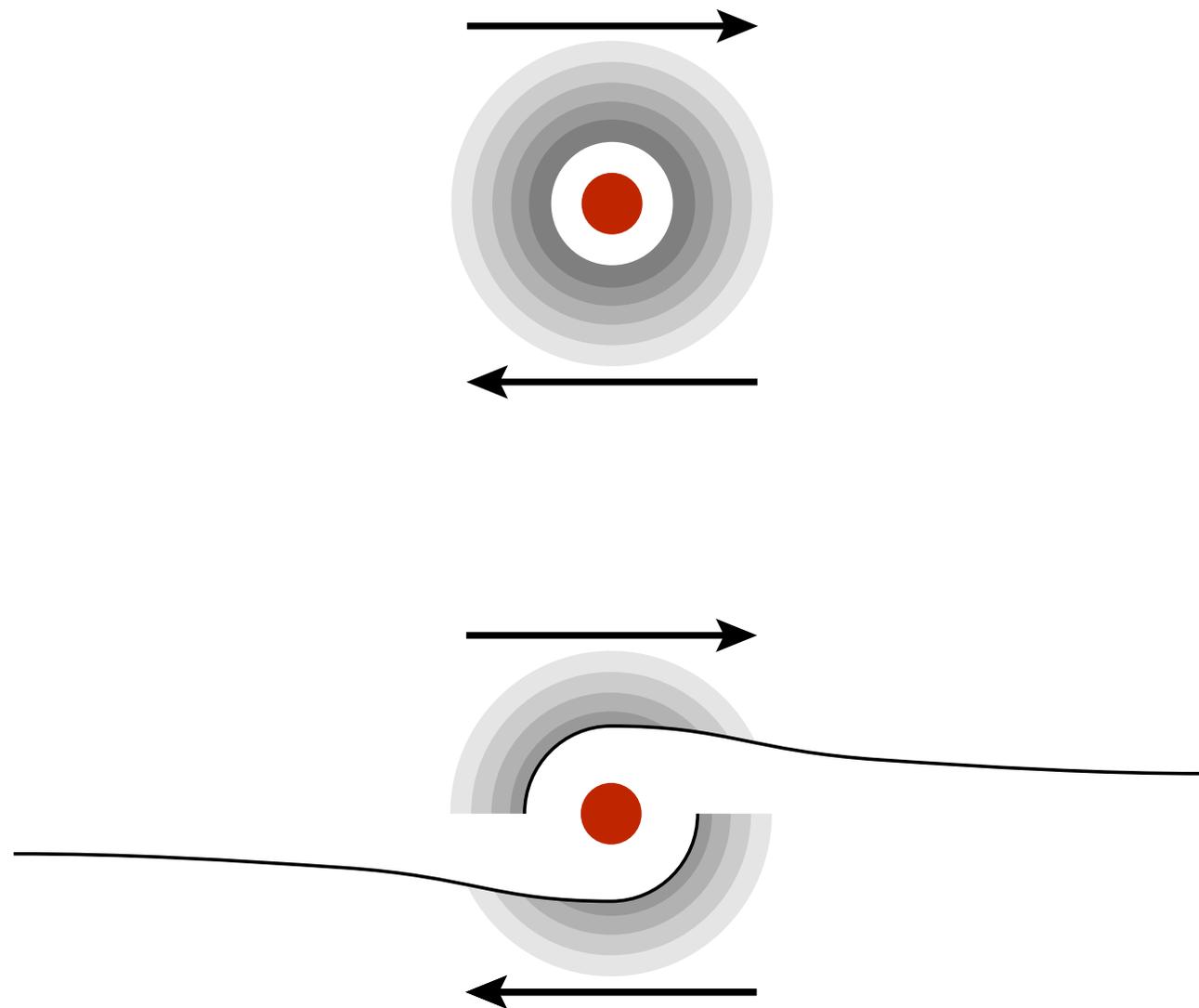
# Effect of Contact: Dilute Suspensions

---



# Effect of Contact: Dilute Suspensions

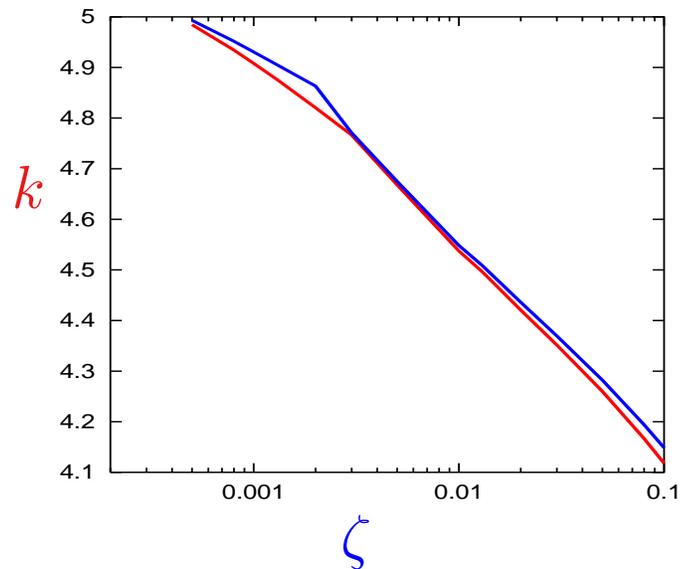
---



## Viscosity of dilute rough suspensions: 2D

Take the effective volume of the system to be a layer of depth  $2a$ .  
 Viscosity (for roughness height  $\zeta > 2.1 \times 10^{-4}$ ) and **rolling** or

**slipping** is  $\eta = \mu \left( 1 + \frac{5}{3}c + kc^2 \right)$ .



- Increasing roughness height **lowers** viscosity
- Changing friction unimportant

# Dense Suspensions: Numerical Simulation

---

## Stokesian Dynamics method

- Brady & coworkers 1988 onwards
- Uses linearity of the Stokes flow problem
- Far-field mobility matrix: invert  $\rightarrow$  resistance matrix with **screening**
- Add exact pairwise resistances

$$\begin{pmatrix} \mathbf{F} \\ \mathbf{T} \\ \mathbf{S} \end{pmatrix} = \left[ \mathcal{R}_{2B} + (\mathcal{M}^\infty)^{-1} - (\mathcal{M}_{2B}^\infty)^{-1} \right] \begin{pmatrix} \mathbf{U} \\ \mathbf{\Omega} \\ \mathbf{E} \end{pmatrix}$$

## Implementing Contact

---

### What do others do?

- Add Brownian motion and a step-function repulsive potential
- Implement a continuous repulsive force over a small range of separations
- ... none of these impose the minimum separation condition

# Implementing Contact

---

## What do others do?

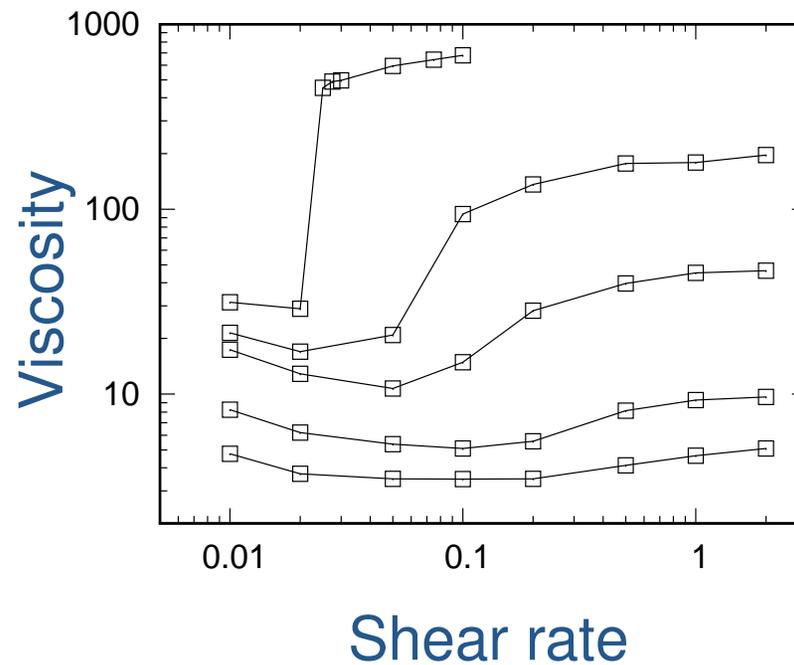
- Add Brownian motion and a step-function repulsive potential
- Implement a continuous repulsive force over a small range of separations
- ... none of these impose the minimum separation condition

## Our approach

- Find normal forces exactly
- Use the linearity of Stokes flow and of SD
- Expand the resistance matrix by one row and column for each contact
- Retain matrix symmetry and positive definiteness
- Approximate tangential force using lubrication theory

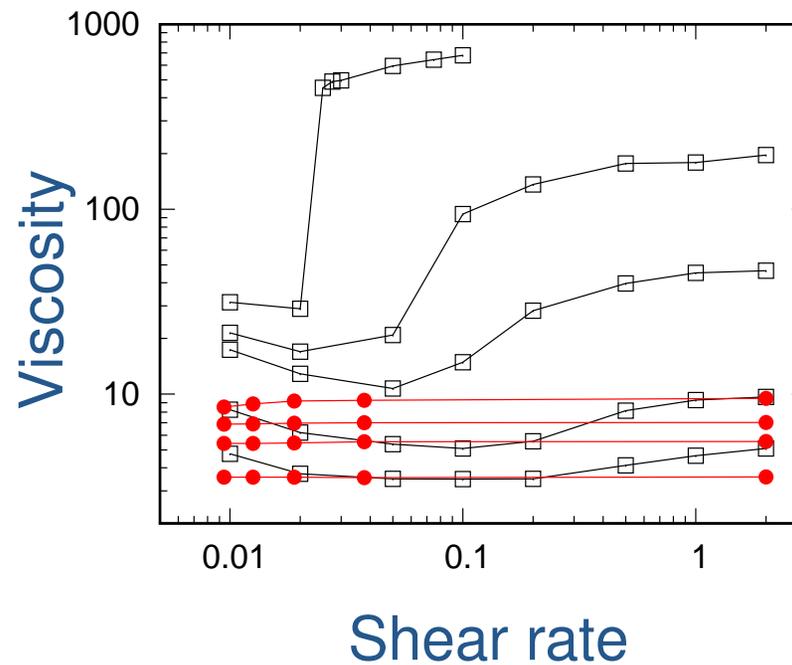
# Shear-thickening with critical load: Results

Literature results (Seto et al)



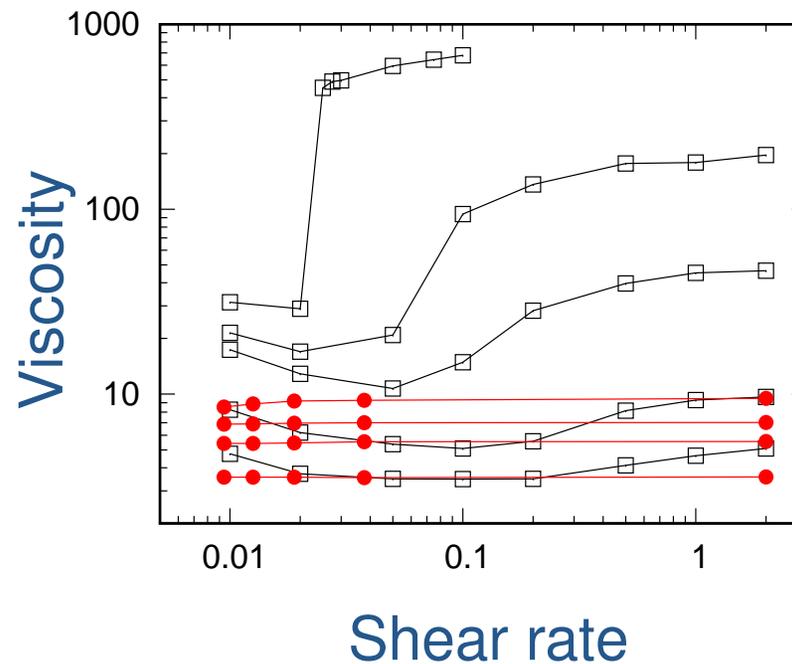
# Shear-thickening with critical load: Results

Literature results (Seto et al) and ours



# Shear-thickening with critical load: Results

Literature results (Seto et al) and ours



- We see very mild thickening (from  $\nu = 0$  to  $F_c = 0$ )
- Not good enough

## Friction and critical load

---

- Low shear viscosity equivalent to  $\nu = 0$
- High shear viscosity equivalent to  $F_c = 0$ , fixed  $\nu$

## Friction and critical load

---

- Low shear viscosity equivalent to  $\nu = 0$
- High shear viscosity equivalent to  $F_c = 0$ , fixed  $\nu$

### Coordination number (Cates, Edwards)

- Low friction, systems should jam at  $Z = 6$  ( $Z = 4$  in 2D)
- Rolling contact systems should jam at  $Z = 4$  ( $Z = 3$  in 2D)
- In 2D, I had to abandon rolling contact for  $c > 0.4$
- Could run with  $\nu = 10$  (still unphysically large)

## Friction and critical load

---

- Low shear viscosity equivalent to  $\nu = 0$
- High shear viscosity equivalent to  $F_c = 0$ , fixed  $\nu$

### Coordination number (Cates, Edwards)

- Low friction, systems should jam at  $Z = 6$  ( $Z = 4$  in 2D)
- Rolling contact systems should jam at  $Z = 4$  ( $Z = 3$  in 2D)
- In 2D, I had to abandon rolling contact for  $c > 0.4$
- Could run with  $\nu = 10$  (still unphysically large)

### Need something else?

- Closer particles to harness lubrication dissipation?
- Compressible asperities

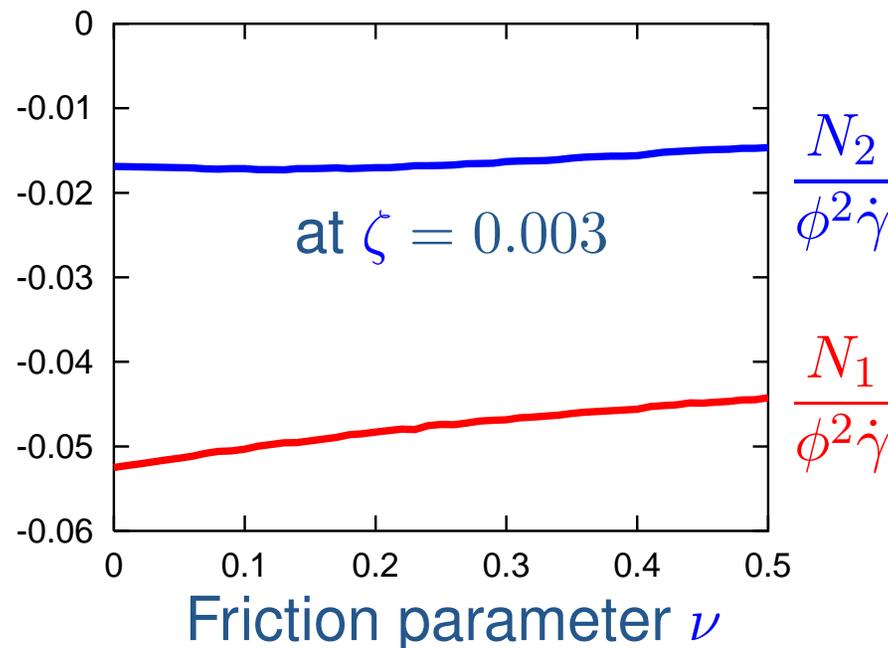
## Normal stress differences: Dilute Suspensions

---

- Can do 3D, since closed orbits don't contribute to  $N_1$ ,  $N_2$
- $N_1$ ,  $N_2$  both zero if  $\zeta < 0.0002$
- Both negative; magnitude increases with  $\zeta$

# Normal stress differences: Dilute Suspensions

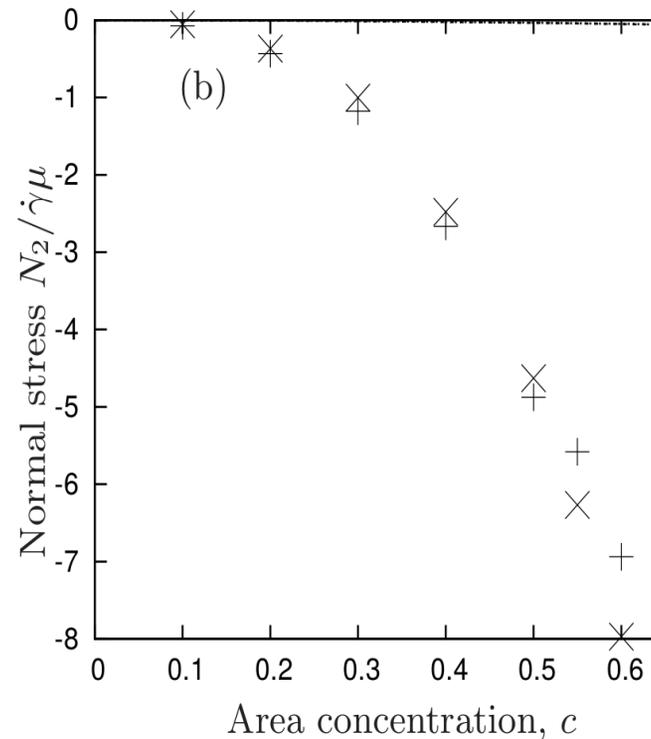
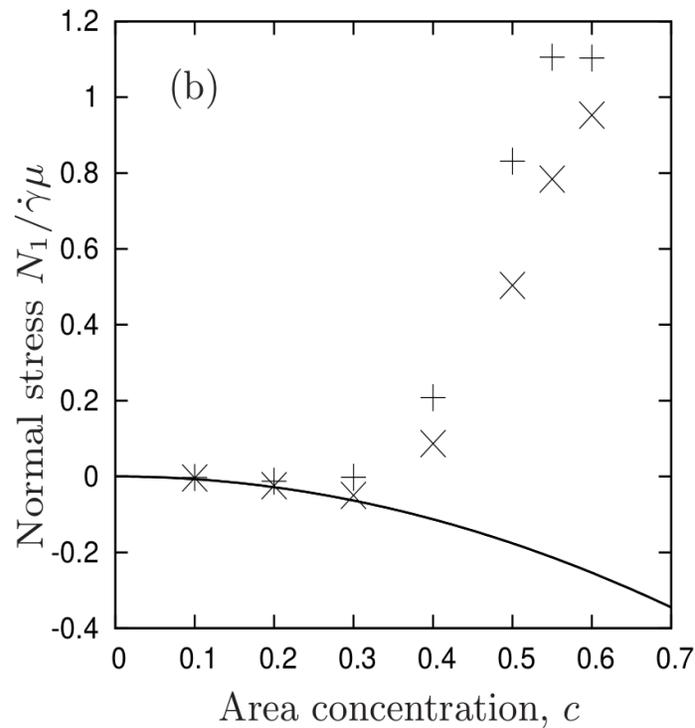
- Can do 3D, since closed orbits don't contribute to  $N_1, N_2$
- $N_1, N_2$  both zero if  $\zeta < 0.0002$
- Both negative; magnitude increases with  $\zeta$



# Normal stresses: Concentrated suspensions

Small 2D simulations using SD. Without (+) and with ( $\times$ ) friction.

- $N_1$  changes sign as concentration increases
- $N_2$  always negative.

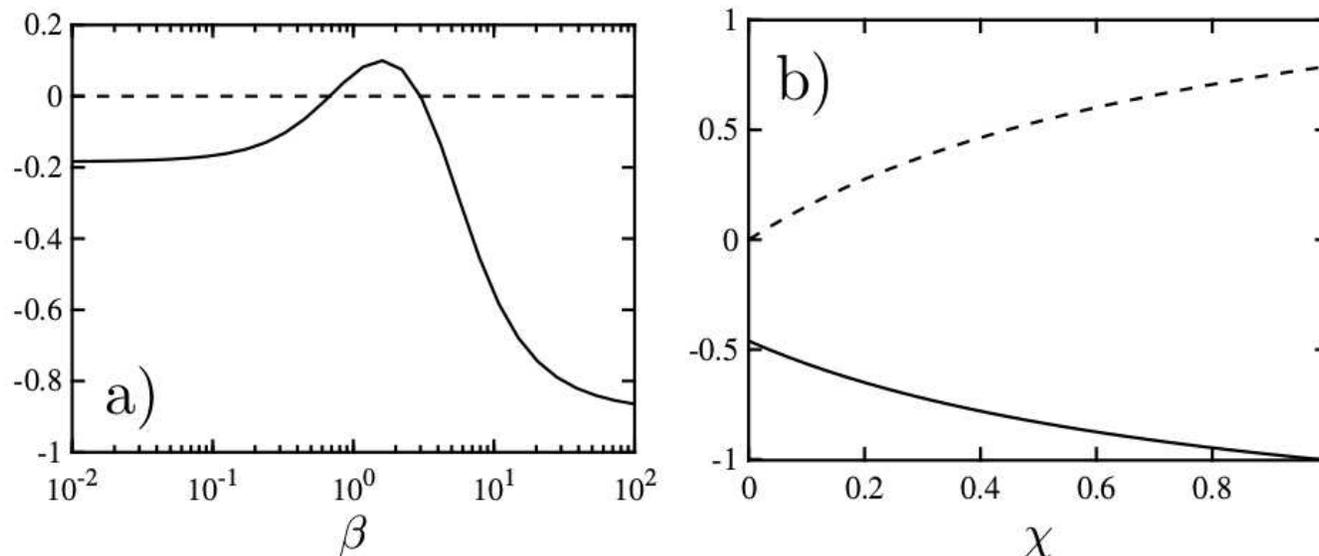


## Normal stresses: Concentrated suspensions model

New constitutive model (Gillissen, PRL, just submitted) for near-jammed suspensions (dominated by pairwise contacts)

- Define stress in terms of moments of pair-vector  $\mathbf{p}$
- Describe evolution of  $\mathbf{p}$  in terms of compressive flux into contact, rotation, and extensional flux out of contact

Predicted  $N_1$  (dashed) and  $N_2$  (solid), scaled by shear stress, without friction (left) and against friction parameter (right):

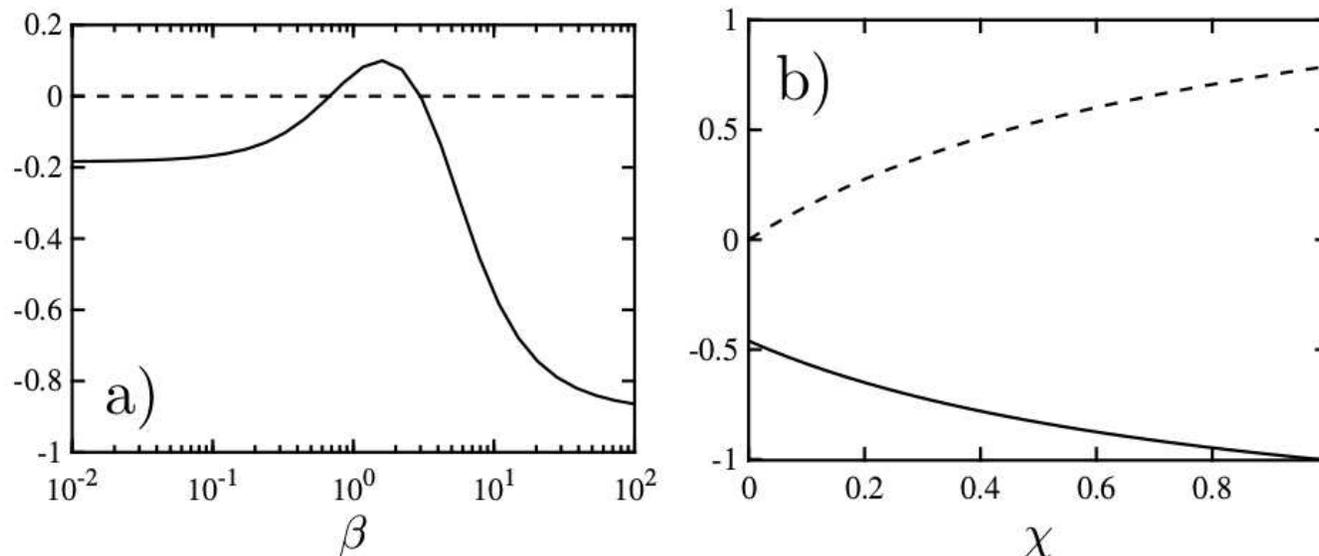


## Normal stresses: Concentrated suspensions model

New constitutive model (Gillissen, PRL, just submitted) for near-jammed suspensions (dominated by pairwise contacts)

- Define stress in terms of moments of pair-vector  $\mathbf{p}$
- Describe evolution of  $\mathbf{p}$  in terms of compressive flux into contact, rotation, and extensional flux out of contact

Predicted  $N_1$  (dashed) and  $N_2$  (solid), scaled by shear stress, without friction (left) and against friction parameter (right):



# Conclusions

---

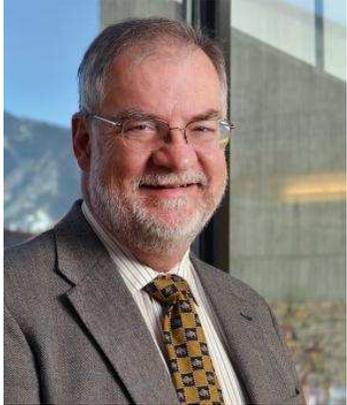
## Viscosity

- Dilute systems:
  - Roughness strongly decreases viscosity
  - Friction weakly increases viscosity
- Dense systems (SD simulations):
  - DST still controversial! Soft contacts?

## Normal Stress Differences

- Dilute systems:
  - Negative normal stresses for  $\zeta > 0.0002$
- Concentrated systems:
  - Simulations:  $N_1$  crossover at higher volume fractions.
  - Jamming:  $N_1 > 0$  caused by friction;  $N_2$  mostly negative.

# Support



Rob Davis – Postdoc advisor – University of Colorado



Adam Townsend – PhD student  
and postdoc – UCL

Jurriaan Gillissen  
Postdoc – UCL



Funding from:



Industrial partner

